

Metal Foams as Compact High Performance Heat Exchangers

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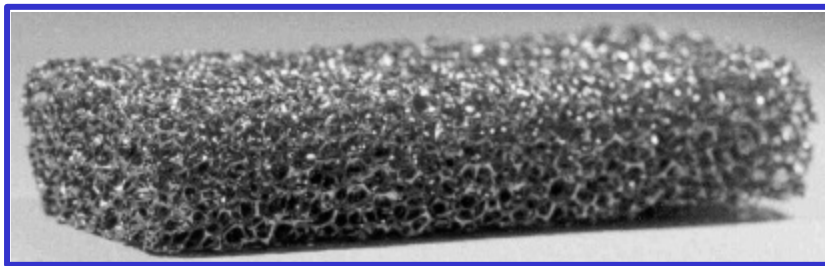
- Thermal management of IGBT's
- Metal foam heat exchanger configuration
- Experiments & Results
- Numerical Simulations
- Structure improvement
- Conclusions

Enhanced Heat Dissipation

- Thermal management of IGBT modules
 - Heat dissipation $+100 \text{ W/cm}^2$
 - Low, uniform operating temperatures increase chip life
- Current configuration
 - Simple flat plate
 - High coolant velocity
 - Significant temperature gradients on the chip
- Possible improvements
 - Implement a highly conductive solid
 - Increase heat convection area
 - Better flow mixing structures

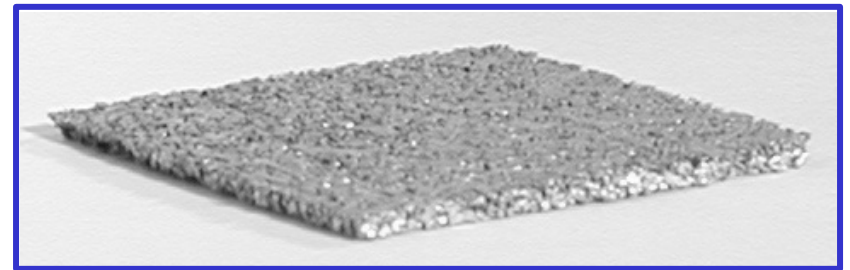
Aluminum Foam Properties

- High surface area to volume ratio
 - $\sim 3000 \text{ m}^2/\text{m}^3$ uncompressed (natural form)
 - $\sim 10,000 \text{ m}^2/\text{m}^3$ compressed
- Highly conductive solid ($\sim 218 \text{ W/m}\cdot\text{K}$)
- Tortuous flow path
- Easily machined to final size



10 cm

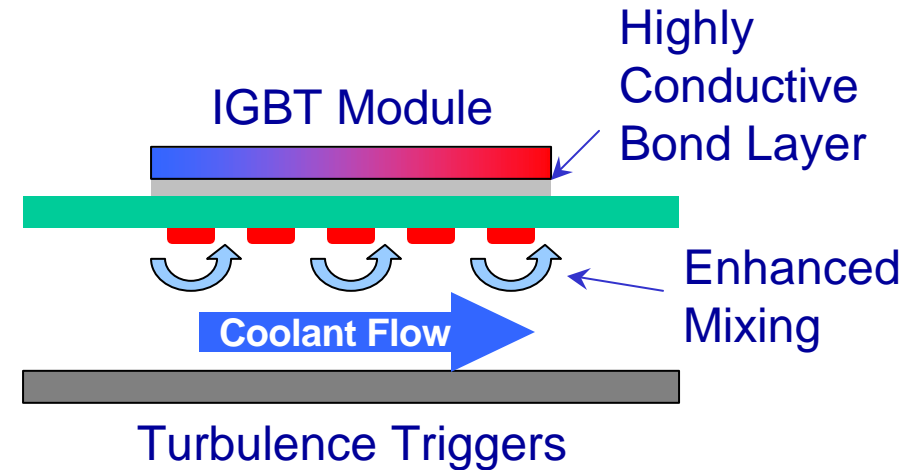
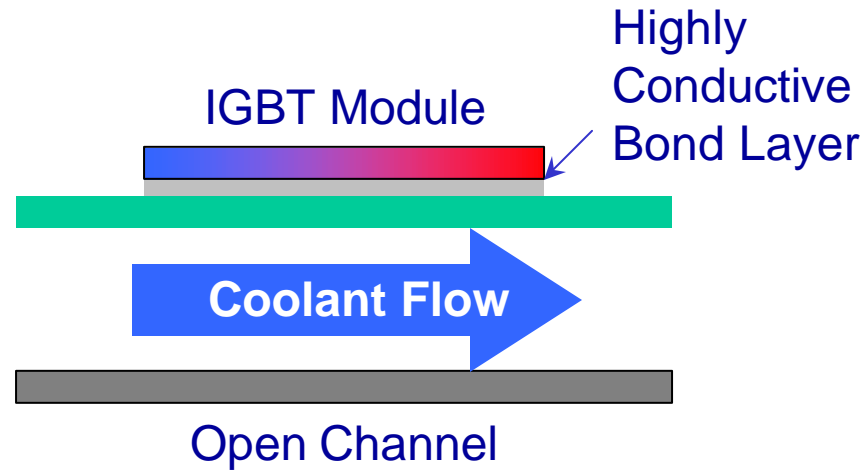
Aluminum foam in as-manufactured,
unaltered state (92% porous)



6.5 cm

Aluminum foam (73% porous)
compressed by a factor of four

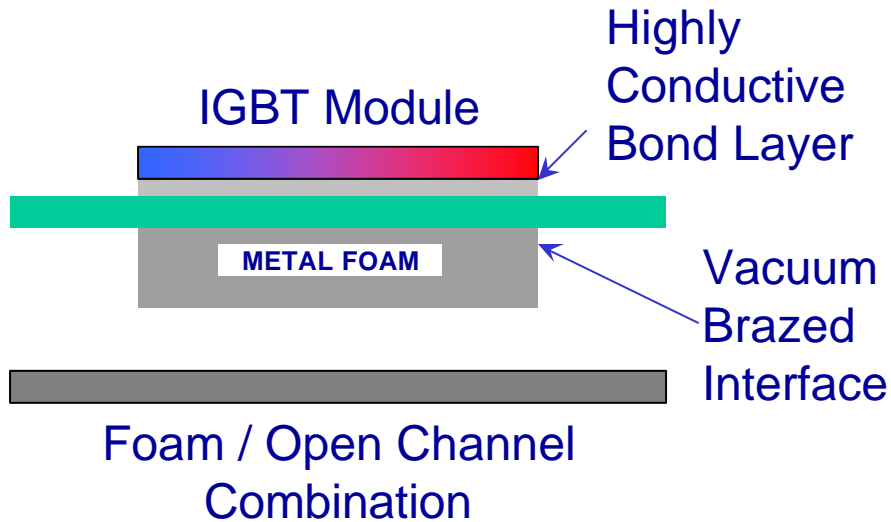
Typical Heat Exchanger Configurations



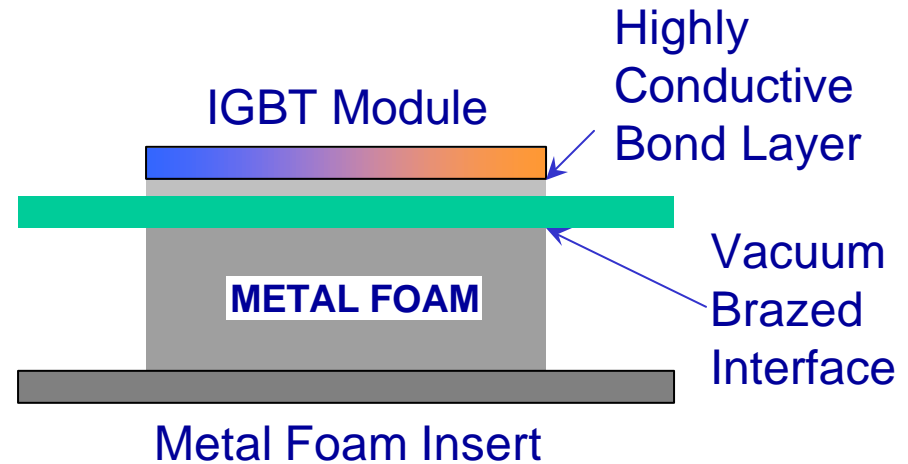
- Simplest design
- High flow velocity
- Mixing depends on upstream channel configuration

- Relatively simple
- Minimal increase in surface area
- Improved mixing through turbulence enhancers

Metal Foam Heat Exchanger Configurations



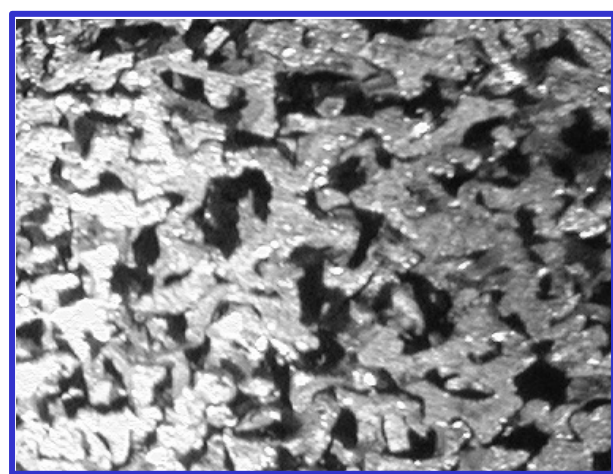
- Similar to turbulence enhancement array
- Lower flow resistance
- Less foam required
- Lower clogging likelihood



- Distributes heat throughout the coolant stream
- Provides a better basis for comparison of metal foam performance data

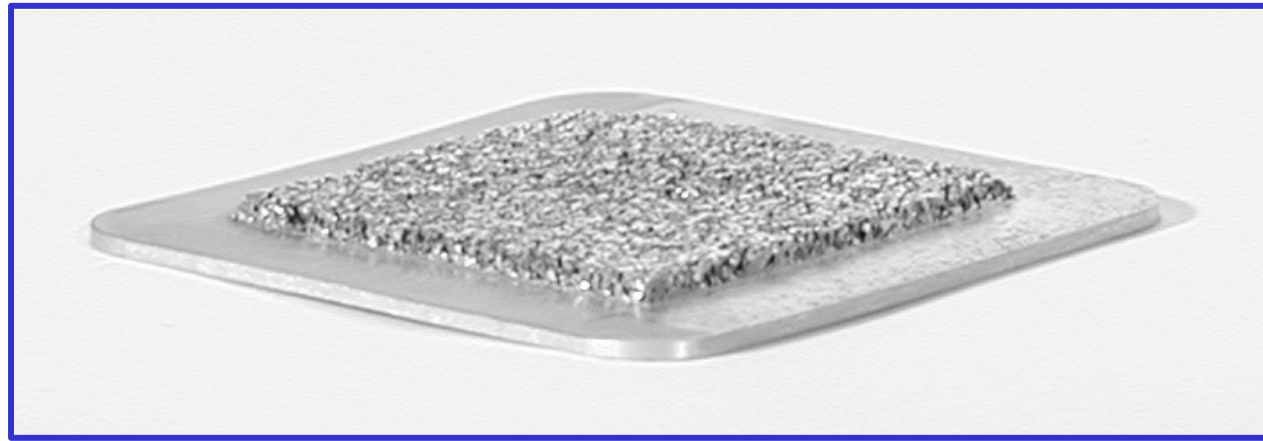
Compressed Foam Experimentation

- Utilize compressed foam—specific surface area $\sim 10,000 \text{ m}^2/\text{m}^3$
- Porosities between 48 – 89%
- Coolant (water) flow velocities up to 2 m/s
- Convection coefficient (measured at plate) $+150 \text{ kW}/\text{m}^2\cdot\text{K}$



2 mm

Compressed Foam Close-up

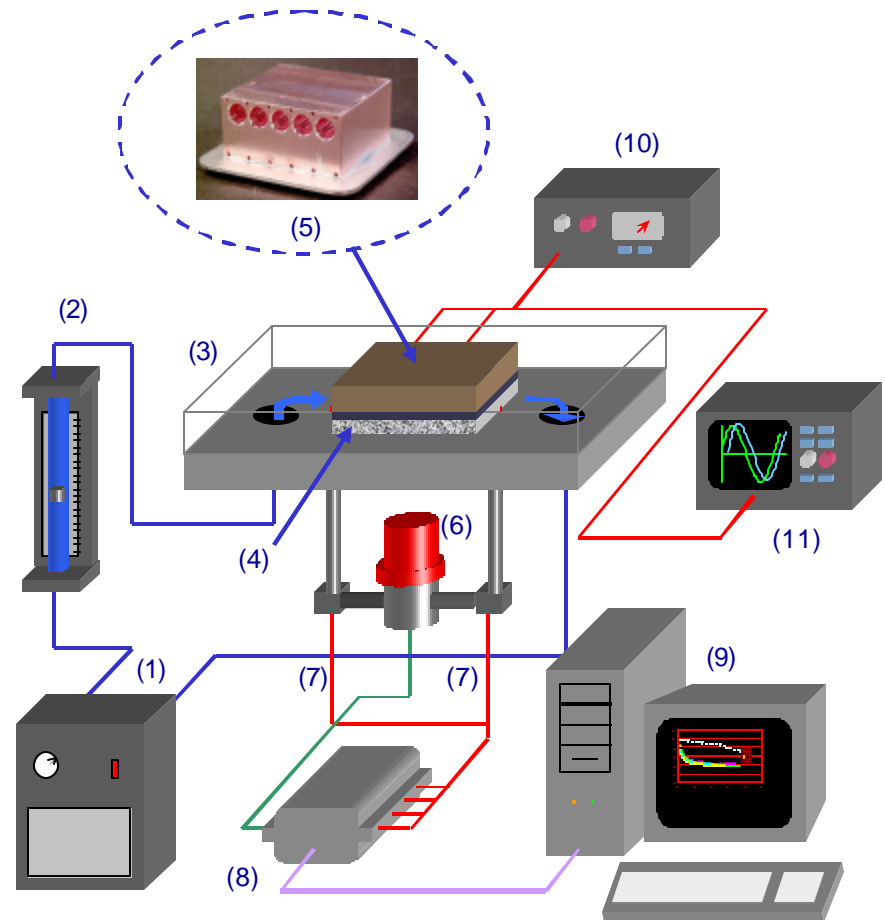


7 mm

Brazed Heater Assembly on a 18% AlSiC plate

Experimental Apparatus

- Pressure drop measurement
- Coolant temperature at various locations
- USB data acquisition device
 - Temperatures
 - Pressure
- 1200 W delivered by cartridge heaters
- Power input
 - Oscilloscope measurement
 - Temperature change in coolant



Pressure Drop and Heat Convection Coefficients

- Forchheimer-extended Darcy equation

$$\frac{\Delta p}{L} = \frac{\mu}{K} v + \frac{c_F}{\sqrt{K}} r v^2$$

c_F Forchheimer coefficient

K permeability

L foam length

v flow velocity

Δp pressure difference

μ dynamic viscosity

r fluid density

- Convection coefficient measured at plate

$$h'' = \frac{\dot{m} c (T_{w,outlet} - T_{w,inlet})}{(T_{plate} - T_{w,inlet}) \bullet A_{foam-plate}}$$

A area

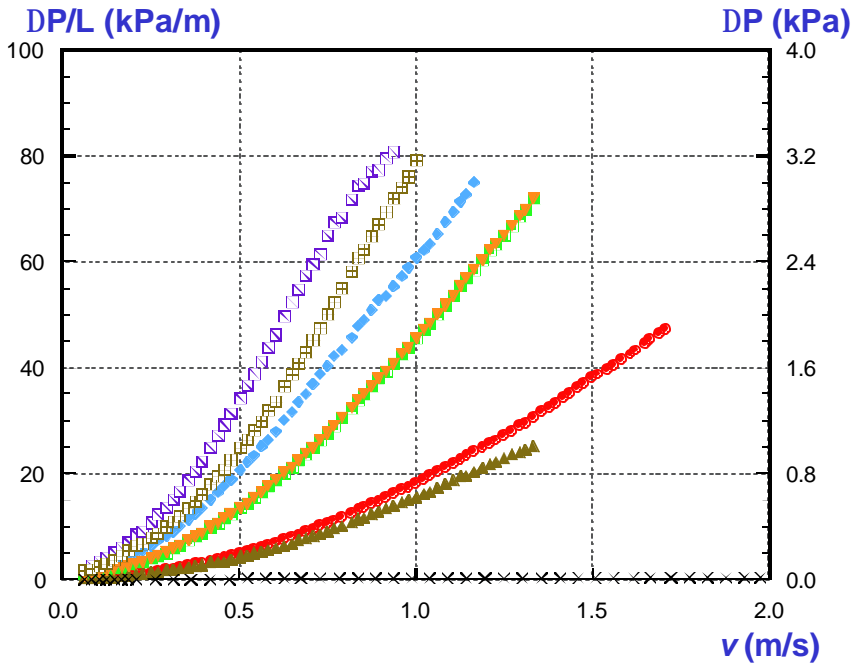
c specific heat

h'' convection coefficient

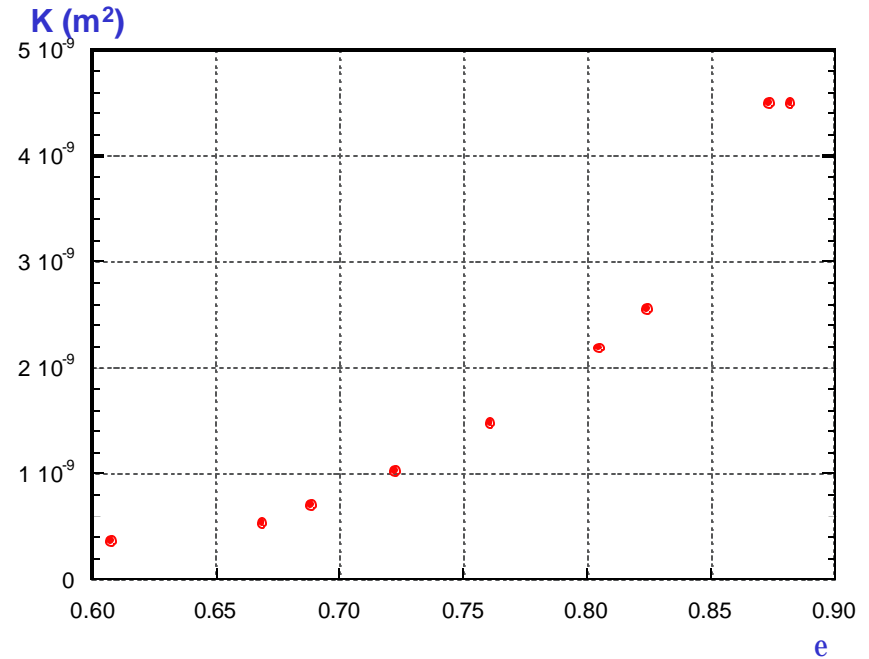
\dot{m} mass flux

T temperature

Flow Characterization Experimental Results

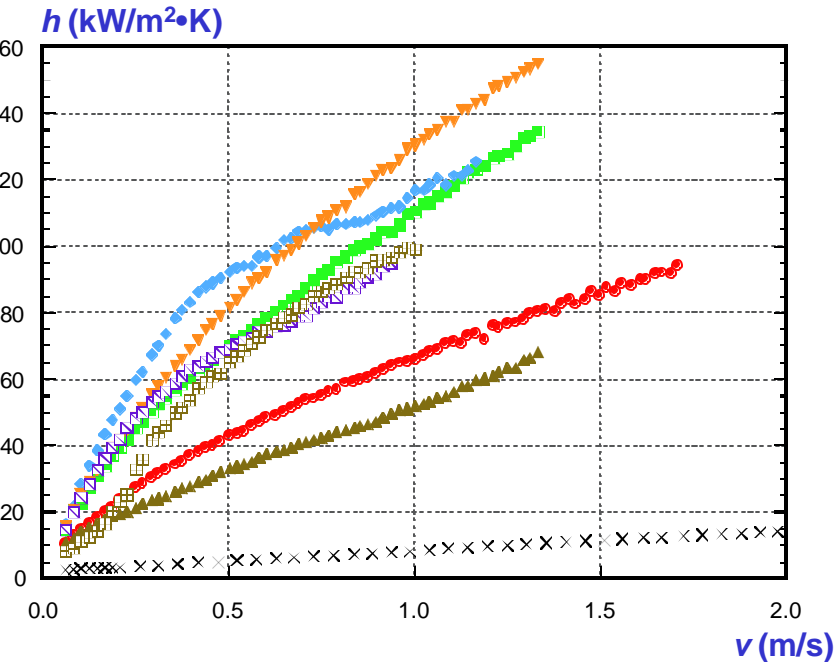


- Porosity decrease = pressure drop decrease
- Significant pressure drop compared to flat plate

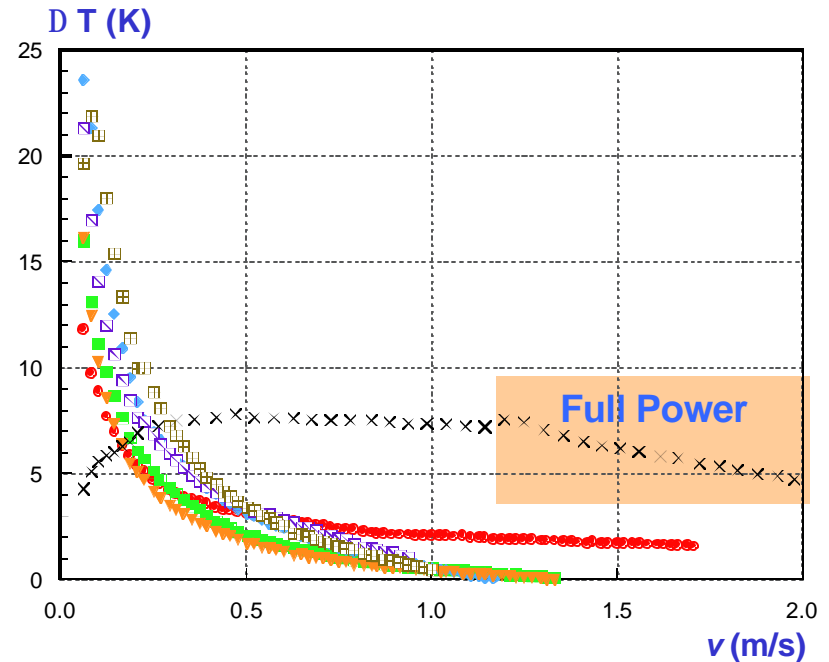


- Monotonic increase of K with porosity
- Increase in sensitivity of K with increase in porosity

Heat Transfer Experimental Results



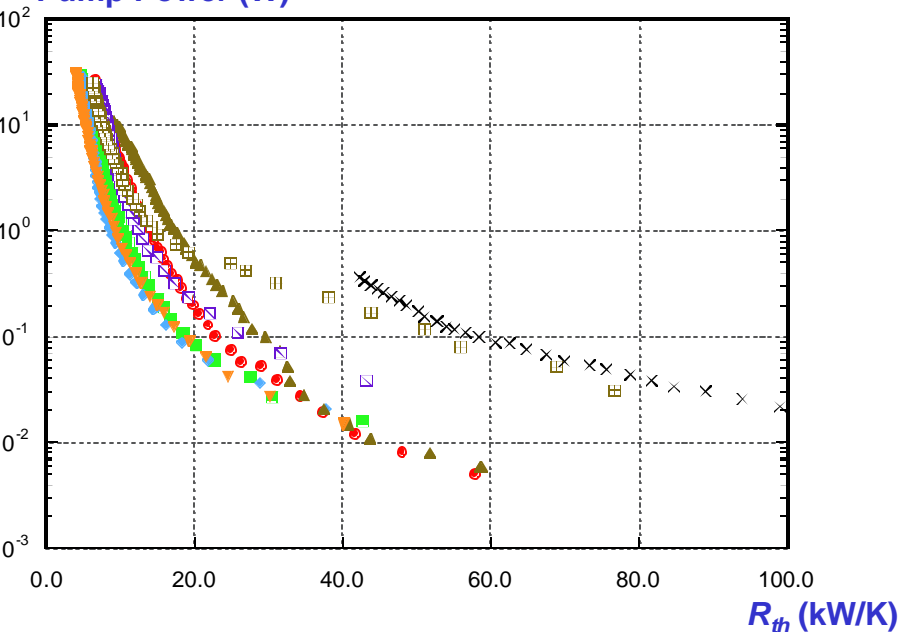
- Higher solid fraction provides a higher heat convection coefficient
- Results are independent of heater attachment



- Control of temperature gradient
- Poor performance by plate
- Note: Limited range for full power for the bare plate

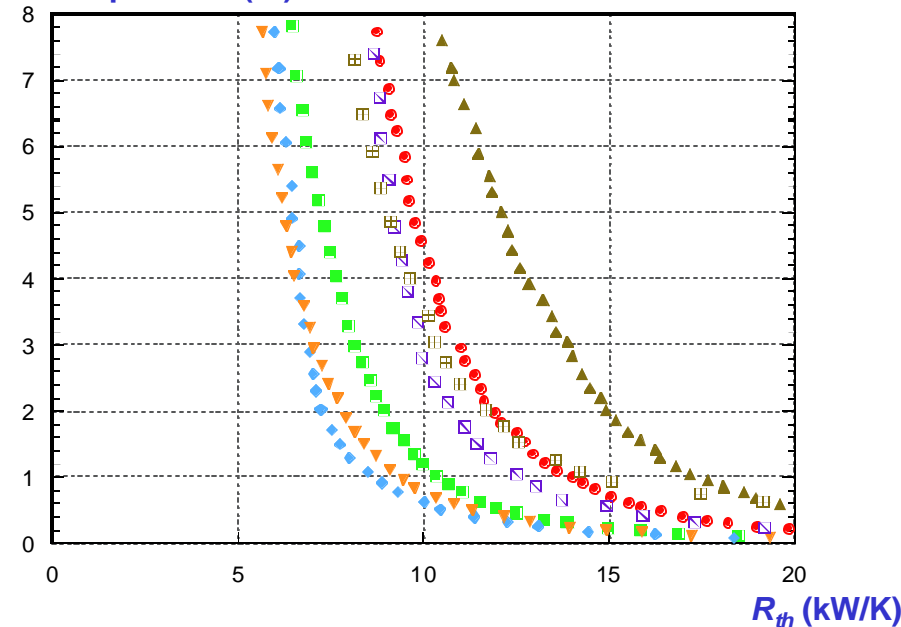
Power-Thermal Resistance Comparison

Pump Power (W)



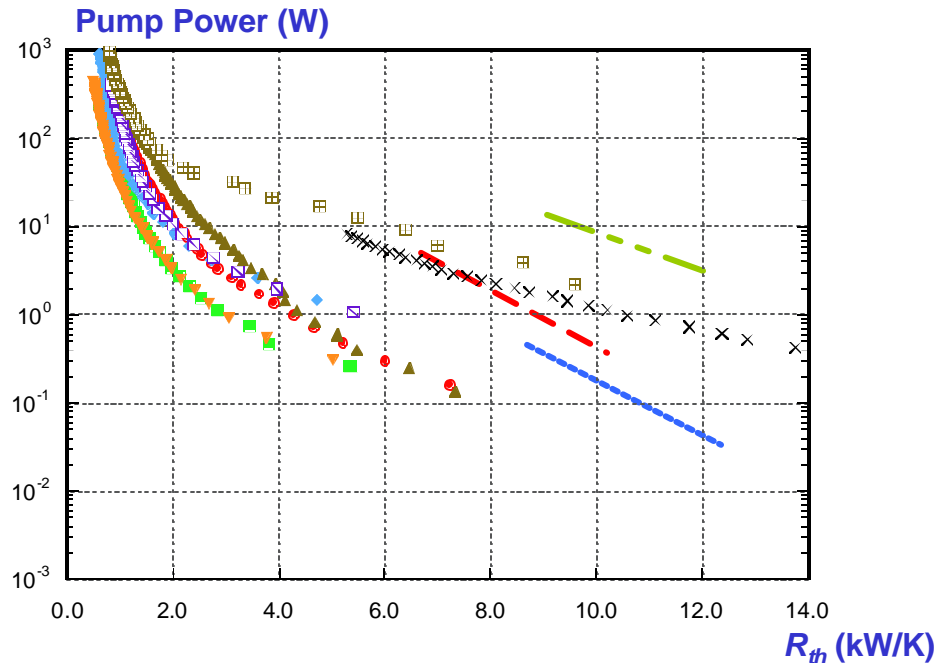
- Basis for real-world performance comparison
- Favorable power—thermal resistance curve
- Poor performance by bare plate

Pump Power (W)



- Locate optimum configuration

Scaled Performance Comparison



Heat Exchanger with Turbulence

0.2 mm Narrow Gap (clear)

Behr Heat Exchanger

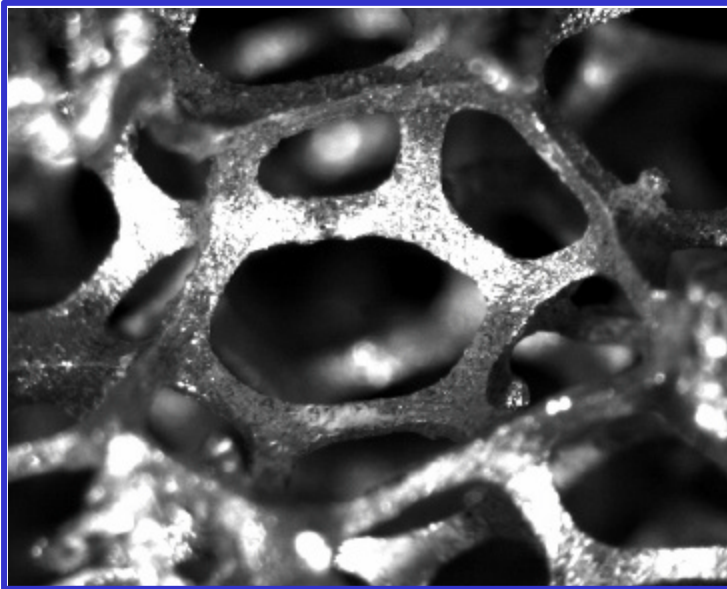
- Scaled to predict behavior with 50% ethylene glycol-water solution
- Assumptions/Considerations
 - Identical K and c_F
 - Similar operating temperature
 - Increase in flow rate compensates lower heat capacitance

Numerical Approaches

- Experimentally measure flow characteristics
 - Requires a wide variety of foam samples
 - Large time expenditure
 - Limited applicability
 - Foam configuration
 - Coolant type & flow rate range
- Pore-based analysis
 - Idealized three-dimensional solid matrix structure
 - Determine periodic flow behavior
 - Calculate interstitial convection coefficient

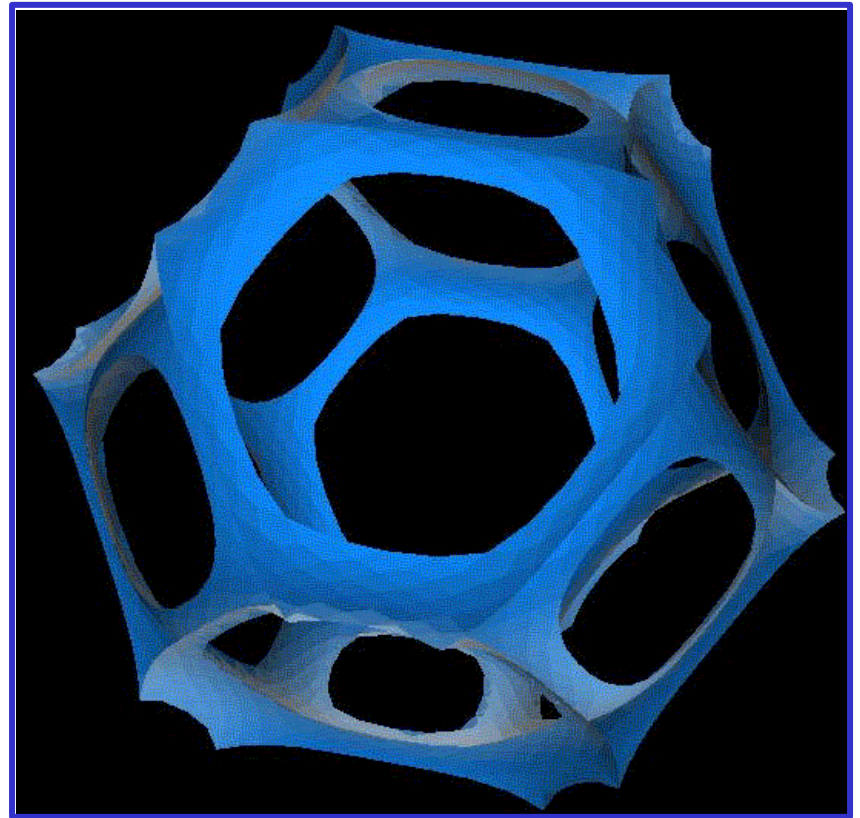
Foam Structure Idealization

- 14-sided tetrakaidecahedron
- Tetrahedral angle ($\sim 109^\circ$)
- Adjustments of shape



5 mm

Close-up of a single open cell



Model of the tetrakaidecahedron

Periodic Cell Boundary Conditions

- Periodic Length L

- Velocity

$$\vec{V}(x, y, z) = \vec{V}(x + L, y, z) = \vec{V}(x + 2L, y, z) = \dots$$

- Pressure

$$p_x(x, y, z) = -Bx + P(x, y, z)$$

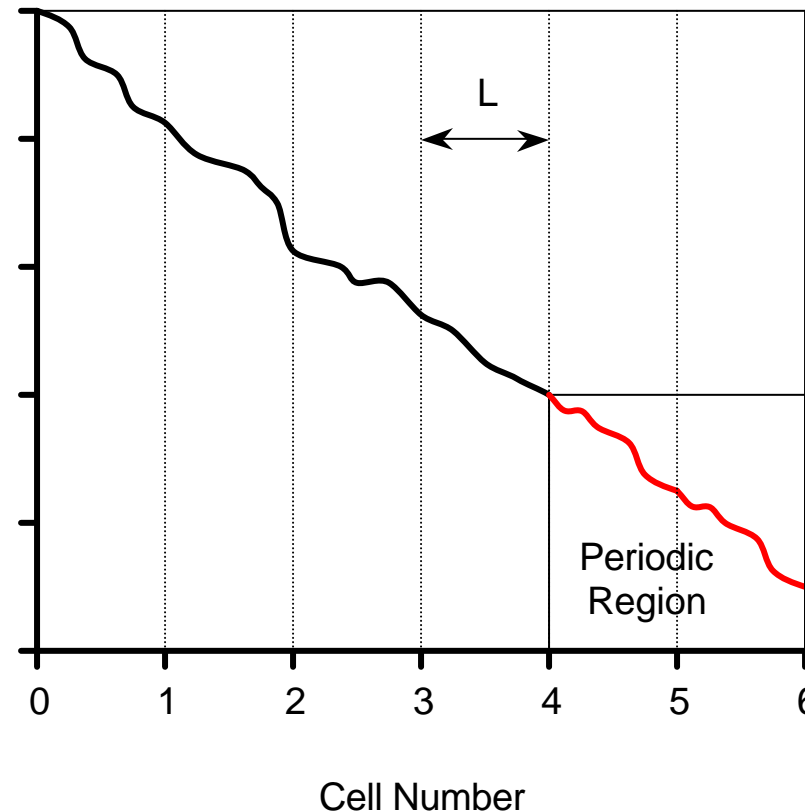
where

$$B = \frac{p_x(x, y, z) - p_x(x + L, y, z)}{L}$$

then

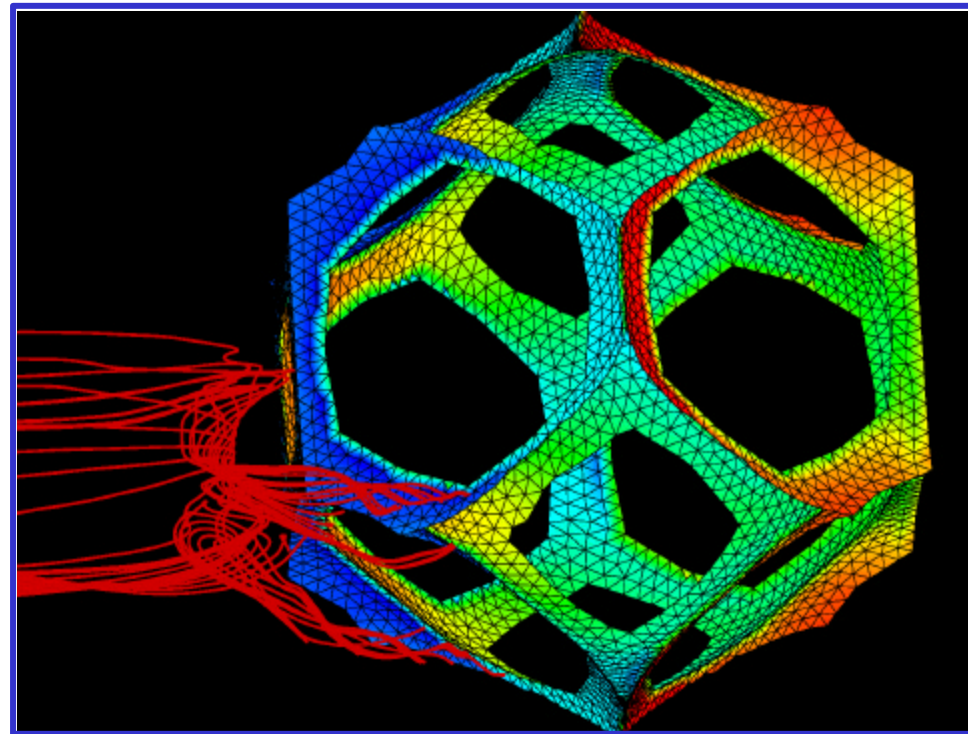
$$p_{y,z}(x, y, z) = p_{y,z}(x + L, y, z) = p_{y,z}(x + 2L, y, z) = \dots$$

Pressure at (x, y_i, z_i)



Visualization of the Flow Field

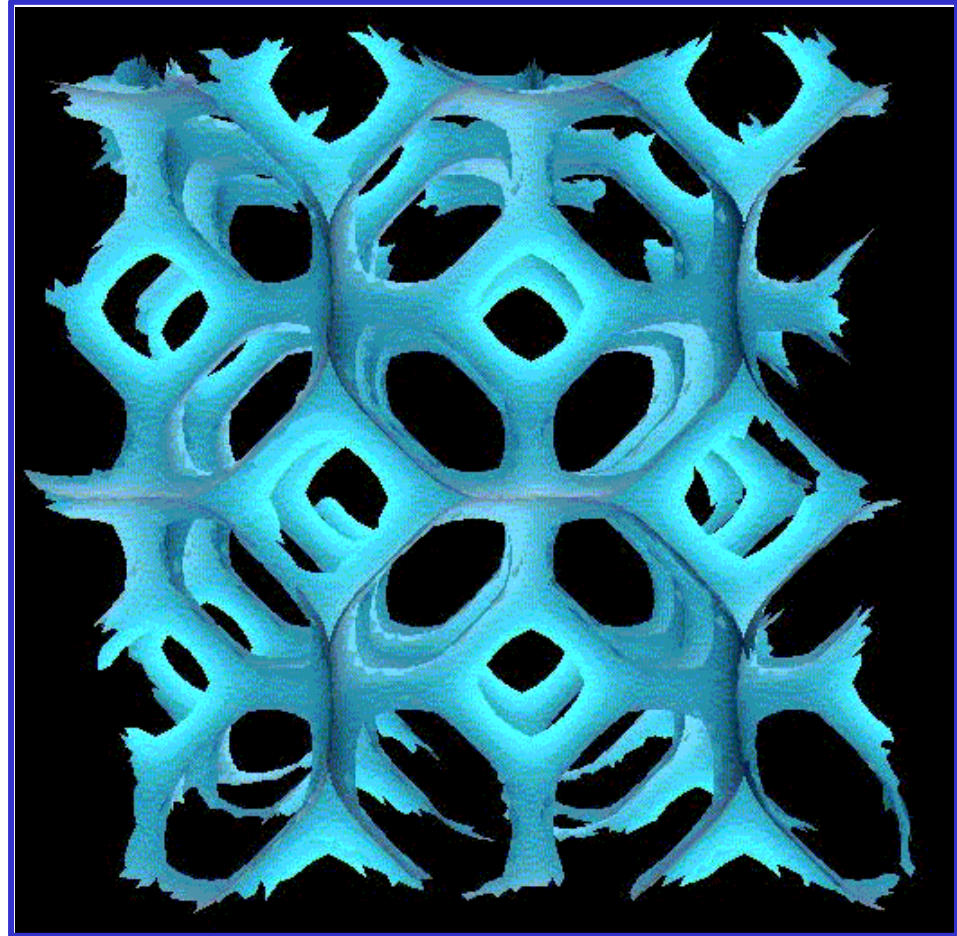
- Colored pressure gradient
- Red particle traces
- Non-turbulent flow
 - $Re_K < 100$ where
 - $Re_K = \rho V K^{1/2} \mu^{-1}$
- Vortex development in wake
 - Describe lack of “transitional range” in porous media
 - Insight into dispersion effects



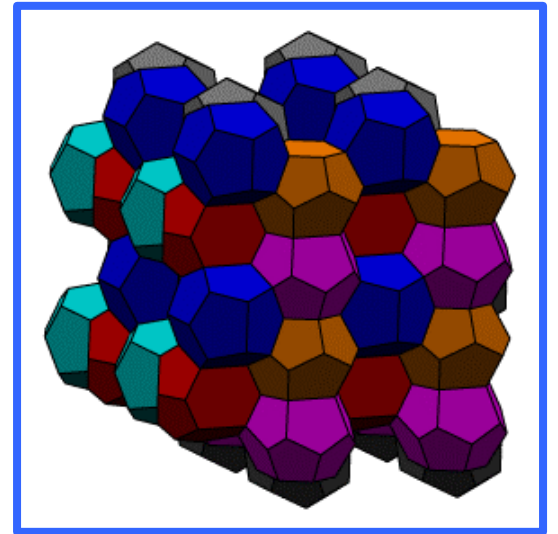
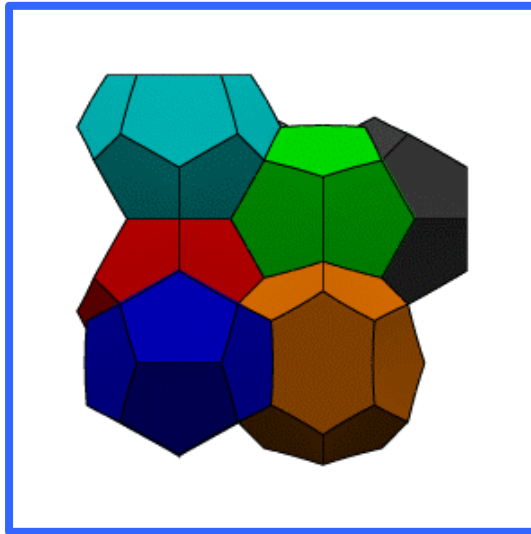
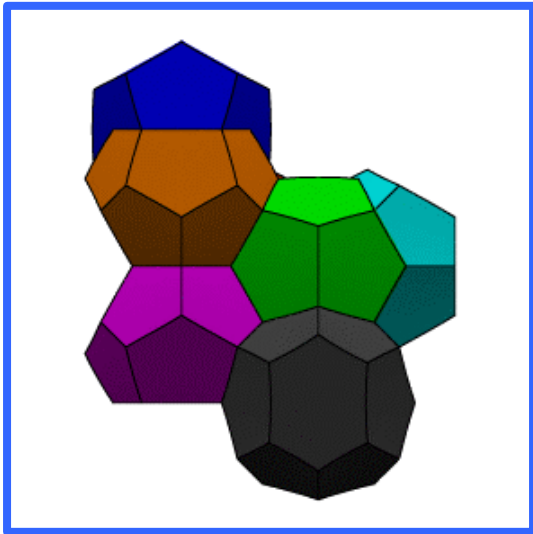
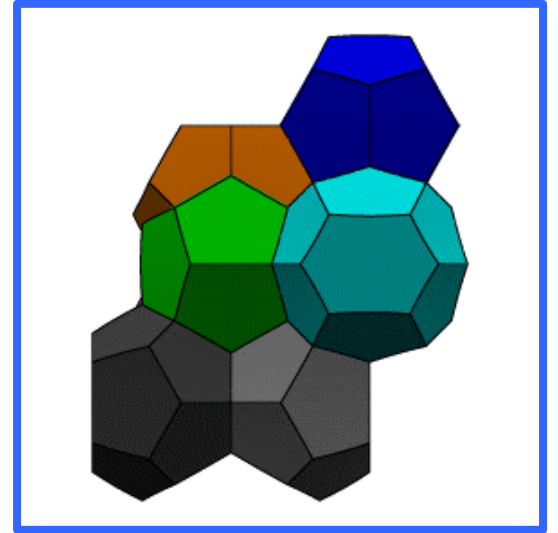
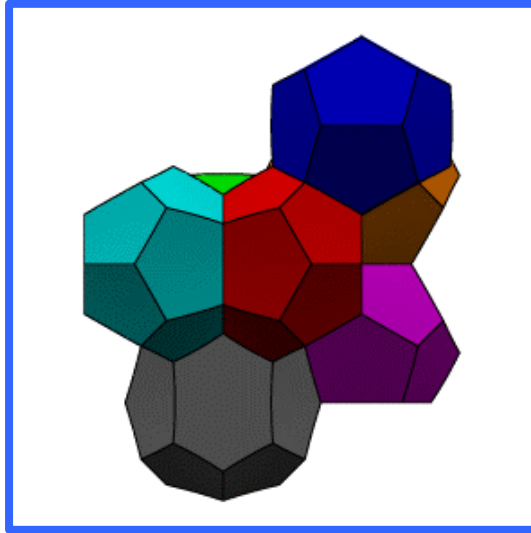
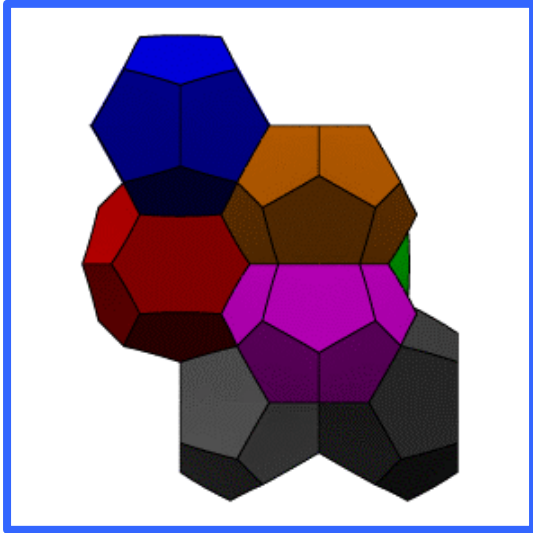
Flow Direction

Periodic Configuration

- Tetrakaidecahedron base unit
- Not numerically optimized to minimize surface energy
- Possible tunneling effects
- Inconsistent porosity
- Improvement needed

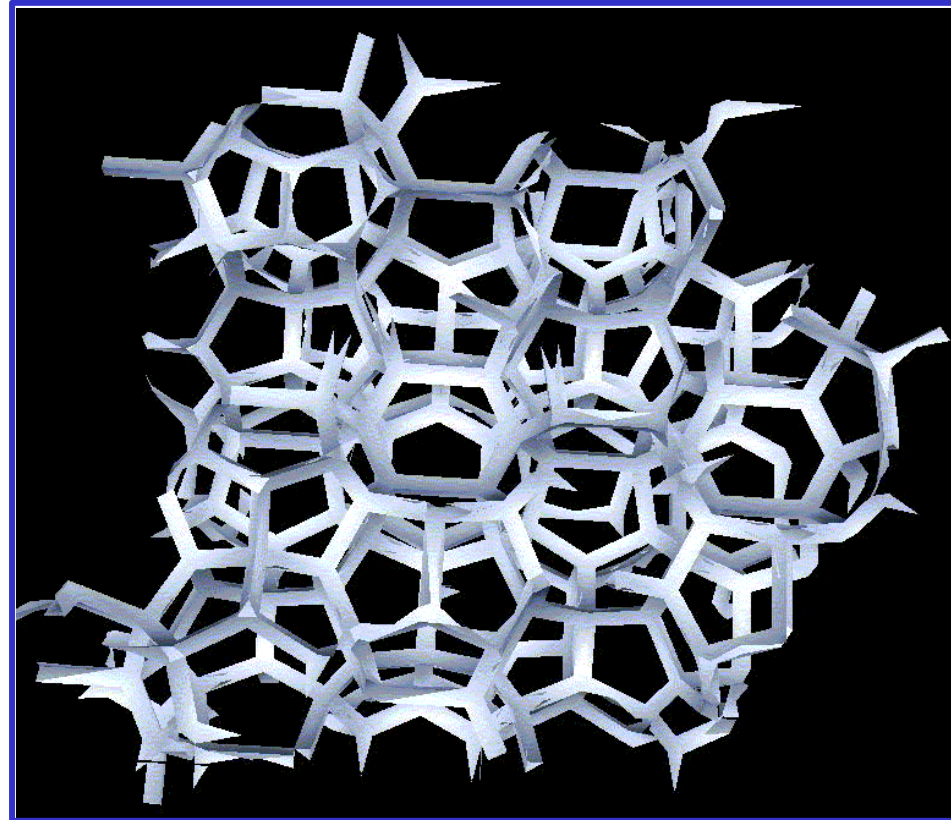


Improvement in Periodic Cell Representation



Wetted Form

- Wetted Weaire-Phelan form
- Numerically optimized surface energy
- 0.3% lower surface energy
- Composition
 - 8 equal volume cells
 - 2 dodecahedra
 - 6 fourteen sided figures
 - 2 hexagonal faces
 - 12 pentagonal faces



Conclusions

- Aluminum foam heat exchanger experiment:
 - Significantly higher heat convection coefficient
 - More uniform chip operating temperature
 - Favorable power input to thermal resistance curve
- Approach of pore-based numerical analysis
 - Analyze “transitional” region in porous media
 - Possibly directly calculate dispersion effects
 - Reduce extensive experimentation